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# Methane capture installation for greenhouse gasses emission reduction in palm oil mill

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**Abstract.** The palm oil industry produces greenhouse gas emissions such as carbon dioxide (CO<sub>2</sub>), methane (CH<sub>4</sub>), nitrous oxide (N<sub>2</sub>O) and other gases through the processing, transportation of vehicles and waste produced. Greenhouse gas emissions can be calculated by the Intergovernmental Panel On Climate Change (IPCC) method. The biggest emission source in the palm oil mill (POM) industry comes from Palm Oil Mill Effluent (POME) and can be reduced by capturing the methane. By making an estimation of greenhouse gases (GHGs) from the operation of the methane capture installation, the total emissions reduced that produced will be known. The palm oil mills that analyzed was a palm oil mill located in Belitung Island, Indonesia. The purpose of this study was to estimate the GHGs emission reduction from the palm oil mill after the installation of biogas methane capture facility. Using IPCC method, the total actual emissions reduction is 70,6%, and without addition of sludge removal in the reactor, the reduction is 84,7%.

**Keywords:** Greenhouse gas emissions, POME, methane capture installation, palm oil industry, IPCC

## 1. Introduction

The current global supply of palm oil comes from Indonesia, and 95% of the land used for plantation is in Sumatera and Kalimantan. According to the Directorate General of Plantations, the Ministry of Agriculture and the Indonesian Palm Oil Association (GAPKI), Indonesia palm oil production has reached 43.9 million metric tons (MMT) in 2018 [1]. When combined with Malaysia, 85% of the world's palm oil comes from both [2]. With this amount, the waste generated from the palm oil industry will also be directly proportional. The wastewater produced in Palm Oil Mill, which is Palm Oil Mill Effluent (POME), contains organic material which, with the microbial activity, will produce methane and carbon dioxide [3].

Without serious treatment, environmental degradation will occur. The high organic content of POME has high potential in polluting the environment in terms of high Chemical Oxygen Demand (COD) and produces Greenhouse Gas (GHG) emissions, therefore special handling is needed to keep the palm oil industry sustainable. Appropriate efforts can be made by making methane capture installation [4].

With the installation of methane capture, electrical energy is produced from anaerobic chemical reaction [5] in POME which becomes methane as generator fuel [6]. Moreover, methane produced can be utilized and not released into the atmosphere. The accumulation of methane that has Global Warming Potential (GWP) 28 will play a role in global warming [7]. The electricity generated from the methane capture installation is green energy to reduce the company's emissions from the use of fossil fuels. Industries that use the methane capture installation can sell the electricity produced to produce profit [8]. Furthermore, the emission at the POM will be reduced. Depth studies need to be done for each company that plans to capture the methane because it needs to be adapted to the design and characteristics of each mill. Even though the palm oil mill industry with the methane capture installation does not process all the POME, the company will still reduce the emissions [9]. In term of the emission produced, the largest emitter is generated from wastewater POME [10].

Based on the above context, the author estimated the GHG emission reduction from palm oil mill that installed methane capture facility (biogas reactor or power plant). The IPCC method applied to analyze the GHG reduction. However, due to the lack of available data, Agriculture, Forestry, and Other Land Use (AFOLU) sector do not include in the calculation. Emission Factor (EF) that used in for energy sector calculation is using the default EF and for waste sector by using industry-specific EF. Results of this study can be used as a consideration for the company to build the methane capture installation or compiling the GHG inventory to report the GHG from palm oil industry.

## 2. IPCC Approach

In order to estimate the GHG of POM, the system boundaries and base year of calculation needed to be fixed. Various data on production of Crude Palm Oil (CPO) and waste generation are needed. Energy consumption from combustion covered in the IPCC method. Biogenic materials that considered as fuel related to process are considered zero. GHGs that IPCC cover are CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub>O for direct emission. CH<sub>4</sub> and N<sub>2</sub>O should be converted into CO<sub>2</sub>eq according to their GWP [11]. The newest GWP can be seen in Table 4.

## 3. Materials and Methods

The method used in this study is from IPCC 2006. GHG was estimated at a processing plant that produces CPO. The company owns a processing plant for CPO, Palm Kernel (PK), Palm Kernel Expeller (PKE), and derived product from refining process i.e. palm olein and palm stearin. The GHG generated quantified from 2012 to 2017.

### 3.1. Data Collection

Energy consumption and fuel consumption data were collected from the company's data. When such data to calculation is not available, GHG estimated based on default IPCC 2006. The baseline year chosen is from 2012 to 2017. The sector to be included in estimation are: 1)energy stationary combustion; 2)energy from mobile combustion; 3)wastewater treatment and discharge. The data source is shown in Table 2.

### 3.2. Calculating the GHG

The net calorific values used to convert the data on fuel consumption from mass units to energy units are provided by the IPCC [12]. The energy sector in POM identified from stationary sources of combustion and mobile sources of combustions. Energy sector calculated by using Tier 1 method of the IPCC [13], with the following equation:

#### 1) Stationary combustion equation

$$\text{Emission (kg/year)} = \text{Energy consumption (TJ/yr)} \times \text{EF (kg/TJ)}$$

Source: [13]

#### Conversion mass unit energy unit

$$\text{Energy consumption (TJ)} = \text{Energy consumption (mass unit)} \times \text{calorific value* (TJ/mass unit)}$$

#### 2) Mobile combustion equation

$$\text{Emission} = \sum \text{Fuel} \times \text{EF}$$

Where the EF is shown in Table 1.

Table 1 EFs of IPCC		
Fuel	Calorific Value*	Sources
Diesel Oil	38x10 <sup>-6</sup> TJ/liter	[14]
Fiber	19,098 KJ/kg	[15]
Shell	20,108 KJ/kg	[15]
Biogas	21,5 MJ/m <sup>3</sup>	[16]
EFB	16 MJ/kg	[17]

#### 3) The waste sector in POM identified from wastewater treatment and discharge. Energy sector calculated by using Tier 2 method of the IPCC [18] with the industry-specific EF. Wastewater

treatment is final process in POM and represents the GHG due to microbial activity occurred in POME. The GHG can be estimated by following the equation:

Total organic degradable material in from industrial wastewater [19]

$$TOW_i = P_i \times W_i \times COD_i$$

where

$P_i$  = total industrial product for industrial sector ton/yr

$W_i$  = wastewater generated, m<sup>3</sup>/ton product

COD = Chemical oxygen demand (plant-specific),

Emission factor for industrial wastewater

$$EF_j = B_o \times MCF_j$$

Total emission from industrial wastewater [19]

$$Emisi\ CH_4 = \sum_i [(TOW_i - S_i) EF_i - R_i]$$

where

TOW : total organically degradable material in wastewater, kg COD/yr

S : organic component removed as sludge inventory, kg COD/yr

i : industrial sector

R : amount CH<sub>4</sub> recovered in inventory year, kg CH<sub>4</sub>/yr

EF<sub>j</sub> : emission factor, kg CH<sub>4</sub>/kg BOD

MCF<sub>j</sub> : methane correction factor

B<sub>o</sub> : maximum CH<sub>4</sub> producing capacity, kg CH<sub>4</sub>/kg COD

Table 2 Data Collection

Data	2012-2013	2013-2014	2014-2015	2015-2016	2016-2017
<b>1A2 Manufacture (biomass)</b>					
Biogas (POME to methcap) (m <sup>3</sup> )	2933431,44	7480873,69	5974563	4799078	5974328
Shell (kg)	24567400	26421400	26362400	22271500	22371870
Fibre (kg)	49134800	52842700	52724800	44543000	44743740
<b>1A2 Manufacture (liquid)</b>					
Solar (genset) (liter)	709120,4	680556	428421	373618	103017
<b>1A3 Transport (liquid)</b>					
Solar (liter)	2729712,67	2935706,67	2929153	2474609	650122,7
<b>4B CH<sub>4</sub> Emission</b>					
Compost (Gg)	0	0	0	2,81377	12,03141
<b>4B N<sub>2</sub>O Emission</b>					
Compost (Gg)	0	0	0	2,81377	12,03141
<b>4D2 TOW Industrial Wastewater</b>					
CPO production (ton/year)	84426,94	92546,09	94695,11	78165,8	76004,17
POME generated (m <sup>3</sup> /ton product)	1,842746223	2,512161782	2,64911639	1,943351901	2,389251116
COD (kg COD/m <sup>3</sup> )	53,529	70,823	71,78	94,15932	91,6136
<b>4D2 CH<sub>4</sub> EF Industrial Wastewater</b>					
Methane producing capacity (kg CH <sub>4</sub> /kg COD)	0,220	0,166	0,164	0,125	0,128
<b>4D2 CH<sub>4</sub> Industrial Wastewater</b>					
Sludge removed (kg COD/year)	0	0	0	2813770	12031400
Recovered CH <sub>4</sub> in each industry (kg CH <sub>4</sub> /year)	0	0	0	0	0

#### 4. Results and Discussion

In the wastewater treatment and discharge sector, there are default emission factors, but in this calculation, the emission factors are used using industry-specific. Waste data obtained from the company will be calculated to find its emission factors, by multiplied Bo with Methane Correction Factor (MCF), which each type of treatment has a different value. The value of Bo depends on the waste COD and the amount of CH<sub>4</sub> produced. the higher the COD value, the smaller the Bo value [11]. Details of the value of Bo for all company calculations and time series can be seen in Table 3.

Table 3 Methane Gas Production from POME in POM

Period	Treatment	Volume POME treated (m3)	COD (kg/m3)	COD (kg)	CH4 Production (ton)	Bo (CH4/COD in kg)
2012-2013	Methcap	116.192	53,53	6.219.627	1.367	0,22
	Open Lagoon	86.548	53,53	4.632.815	2.385	0,22
2013-2014	Methcap	296.315	70,82	20.985.946	3.486	0,17
	Open Lagoon	6.653	70,82	471.195	3.565	0,17
2014-2015	Methcap	90.253	71,78	6.478.379	2.784	0,16
	Open Lagoon	236.651	71,78	16.986.798	3.846	0,16
2015-2016	Methcap	190.090	94,16	17.898.764	2.237	0,12
	Open Lagoon	7.862	94,16	740.267	2.329	0,12
2016-2017	Methcap	236.642	91,61	21.679.585	2.784	0,13
	Open Lagoon	-	91,61	-	2.784	0,13

The emission calculated then need to be converted into CO<sub>2</sub>eq. CH<sub>4</sub> and N<sub>2</sub>O converted based on their GWP. The following GWP those gases can be seen in Table 4 and the result of GHG emission calculation is shown in Table 5:

Table 4 Global Warming Potential

Gases	GWP
CO <sub>2</sub>	1
CH <sub>4</sub>	28
N <sub>2</sub> O	265

Source : [7]

Table 5 Total Emission

Keterangan	2012-2013	2013-2014	2014-2015	2015-2016	2016-2017
Total Emission Gg CO <sub>2</sub> e	32,62	12,07	33,37	10,70	4,26

Total emissions tend to decrease from year to year. The greater the POME produced, the greater the emissions, but if the CH<sub>4</sub> is capture in methane capture installation (biogas reactor) the emissions are saved. In the 2015-2016 and 2016-2017 periods, the calculation of waste emissions will be reduced by sludge removed. From 2015 to 2016 and 2016-2017 the emission value will decrease due to sludge utilization activities which will affect the amount of Wastewater TOW. The smallest emission value occurred in the period 2016-2017 due to all POME produced was entered into the Biogas Power Plant, so there are no emissions from open ponds (emissions only come from burning fossil fuels). Table 6 shows the percentage reduction of GHG emissions.

Table 6 Reduction of Emission

Period	Energy emission (Gg CO2e)	Open Lagoon Emission (Gg CO2e)	Methane capture Emission (Gg CO2e)	Total Waste Emission (Gg CO2e)	Total Emission (Gg CO2e)	Percentage of reduction (%)
	A	B	C	(B+C)=D	(A+B)=E	(C/D)*100
2012-2013	9,808	22,810	30,623	53,434	32,619	57,311
2013-2014	10,316	1,753	78,097	79,850	12,070	97,804
2014-2015	9,585	23,787	62,372	86,159	33,373	72,392
2015-2016	8,625	9,948	42,224	52,172	18,573	80,932
2016-2017	4,263	34,613	27,756	62,369	38,875	44,504
					Average	70,588

Table 6 shows the number of emissions from the energy and waste sectors. The company has a sludge removal system starting in the 2015-2016 period. The amount of energy sector emissions is affected by the number of fossil fuels used both in the process and in transportation. The longer the distance between the plantations, the more fuel consumption, and the greater emissions. In this case, POME waste will enter the methane capture installation and the rest will be processed in an open lagoon. The waste emissions mentioned in table 6 come from the emissions of waste discharged into the open lagoon. Methane capture emissions come from emissions produced by methane capture installations, but they do not add up to total emissions because they include biogenic materials to produce energy. Then emissions from open lagoon full are emissions if all waste is processed into an open lagoon. These emissions are calculated to determine the reduction of emissions from the operation of the methane capture installation. The total emissions are the actual value of the total emissions from the energy and waste sector emissions.

The amount of energy emissions based on the use of fossil fuels tends to decrease because the transportation distance is also reduced. Waste emissions tend to fluctuate with large differences. That is because not all POME is processed into methane capture installation. In the period 2015-2016 and 2016-2017, it did not originate from POME emissions which were processed in the open lagoon, but also from sludge removal as well. Methane capture emissions tend to increase then decrease, the decrease is due to sludge removal. Because in the calculation, the emissions in the methane capture installation will be reduced by the correct amount of sludge removal. Open lagoon full emission is total emissions from waste, but this is not an actual condition. The amount is influenced by the amount of POME produced. The company's actual emissions can be known from the total emission from sectors of energy and waste. The average emission reduction is 70.588%, but to find out the emission reduction from the operation of the methane capture installation it is necessary to eliminate the variable sludge removal (Table 7).

Table 7 Reduction of Emission (without sludge removal)

Period	Energy emission (Gg CO2e)	Open Lagoon Emission (Gg CO2e)	Methane capture Emission (Gg CO2e)	Total Waste Emission (Gg CO2e)	Total Emission (Gg CO2e)	Percentage of reduction (%)
	A	B	C	(B+C)=D	(A+B)=E	(C/D)*100
2012-2013	9,808	22,810	30,623	53,434	32,619	57,311
2013-2014	10,316	1,753	78,097	79,850	12,070	97,804
2014-2015	9,585	23,787	62,372	86,159	33,373	72,392
2015-2016	8,625	2,072	50,100	52,172	10,697	96,028
2016-2017	4,263	-	62,369	62,369	4,263	100,000
					Average	84,707

In table 7, a calculation is made if sludge removal is not taken into account to obtain a reduction in emissions only from the methane capture installation. The number of waste emissions in the period 2015-2016 and 2016-2017 came from POME waste obtained at the open pond only. From 2016 to 2017 the number of emissions is zero because all the POME entered is processed into the methane capture installation entirely. By doing this calculation, it can be known as actual methane capture emissions so that emissions reductions



can be discovered. The average emission reduction from the operation of the methane capture installation was 84.707%.

## 5. Conclusions

The conclusions obtained are:

1. The results of the calculation of total emissions using the IPCC method are greatly influenced by the amount of POME produced and the method of processing the POME (whether using a methane capture installation or not).
2. By using methane capture installation, GHGs emission reduction is 84.7% (without sludge removal from the biogas reactor).
3. The actual GHGs emission reduction using methane capture installation is 70.6% with sludge removal is taken into account.

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